

Integrated Surface Dynamics for SPH-based Fluid Simulation

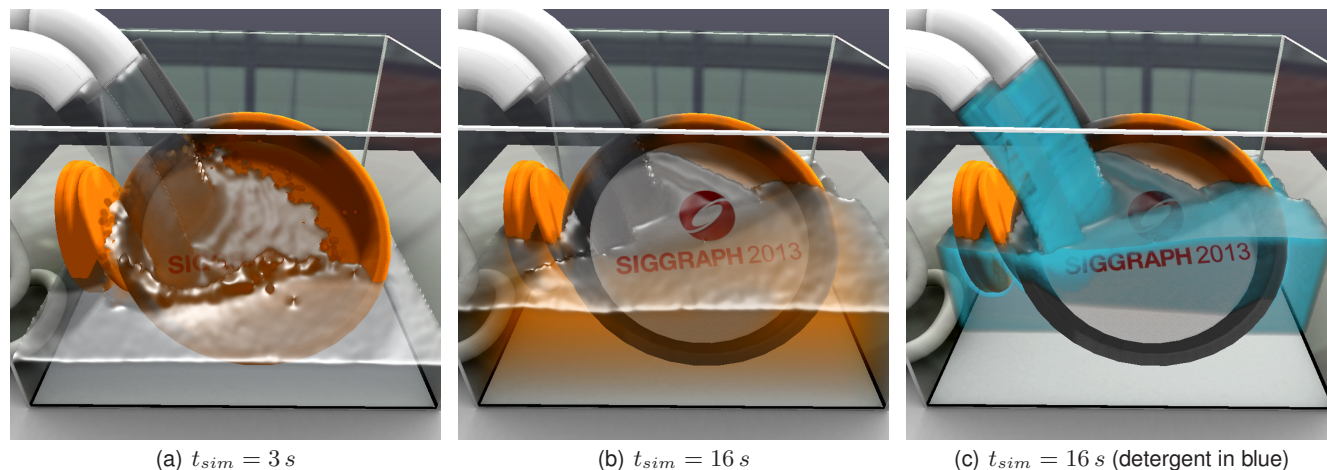


Figure 1: The pan’s surface is cleansed from grease (orange) due to detergent concentration (blue in 1(c)) on the fluid’s surface.

Abstract

Surface dynamics play an essential role in fluid simulations. A vast number of effects including wetting of surfaces, cleansing, and foam dynamics are based on surface-surface and surface-bulk interactions, which in turn rely on a robust surfaces computation.

In this paper we introduce a conservative Lagrangian simulation of surface dynamics based upon incompressible smoothed particle hydrodynamics (SPH). The key concept of our approach is to realize surface dynamics using an implicit definition of the fluid’s (free) surface. Our algorithm assigns a scalar particle value estimating the surface area of each particle. Based on this implicit surface definition, surface dynamics are incorporated using scalar particle quantity concentrations in the bulk and at the surface. Transport of quantities between bulk and surface is simulated by introducing a symmetric, conservative SPH-based formulation of the Langmuir-Hinshelwood adsorption mechanism.

We demonstrate two different types of surface-relevant effects: diffusion on surfaces and reaction kinetics. Reaction kinetics model the dynamics at fluid interfaces based on transition rules between different quantities in order to realize effects like cleansing.

CR Categories: I.3.5 [Computer Graphics]: Computational Geometry and Object Modeling—Physically based modeling I.3.7 [Computer Graphics]: Three-Dimensional Graphics and Realism—Animation

Keywords: fluid simulation, SPH, surfaces dynamics, surfactants

1 Introduction

Lagrangian fluid simulation using smoothed particle hydrodynamics (SPH) is a well established method. Major advantages of this approach are mass conservation and the simple handling of free surfaces. There is a vast SPH literature, e.g. providing extensions of the SPH simulation model in order to realize complex dynamic boundaries [Akinci et al. 2012b], bulk transport of soluble substances [Kristof et al. 2009], multi-phase simulations [Solenthaler

and Pajarola 2008], tracking [Adams et al. 2007] and capturing of surfaces [Akinci et al. 2012a].

Effects on complex fluid surfaces and interfaces are a basic element of many applications in Computer Graphics. Several SPH-based methods have been introduced in this respect, e.g. the convection of diffuse materials [Losasso et al. 2008], dynamics of foam [Ihmsen et al. 2012], and multiple-phase scenarios [Losasso et al. 2006; Solenthaler and Pajarola 2008; Akinci et al. 2012b].

Surface dynamics supplement fluid dynamics, e.g. on small scales the can even dominate convective flux. However, considering conservative Lagrangian surface dynamics, there is little research until now. Particle level set (PLS), for example, use particles to track flow details, e.g. Losasso et al. [2008] use a PLS-SPH combination to model surface effects like foam and spray. However, PLS in general cannot fully conserve mass at free surfaces and Losasso et al. [2008] did not incorporate transport mechanisms between surface and bulk. Semi-Lagrangian contouring methods, on the other hand, are used for tracking of surface characteristic, e.g. color and texture coordinates, like Bargeil et al. [2006], but maintaining an explicit polygonal mesh is expensive and surface dynamics are complicated to integrate.

Thus, to the best of our knowledge, for SPH-based fluid simulations there has been no formulation for conservative transport mechanisms within a fluid’s surface and between surface and fluid volume (bulk), which, for example, are required to model the dynamics of detergents as shown in Fig. 1.

Detergents themselves belong to the wider class of materials called surfactants (surface active agents), which exhibit different behavior on surfaces and in the bulk, i.e. often they get attracted to the surface, rather than remaining in the bulk. Surfactants are widely used in chemical and biological applications, including wetting phenomena [Fell et al. 2011], cleansing action [Rosen and Kunjappu 2004], and drug delivery [Dekker 2002].

Note, that we will use the notion of surface dynamics and surfactants dynamics interchangeably throughout this paper, even though surface dynamics could involve further concepts.

Contribution: In this paper we present a novel SPH-based fluid simulation approach with integrated surface dynamics. The main contributions of our work can be summarized as follows:

- We introduce a reliable computation of surface areas for individual particles, which is the essential foundation for any surface dynamics (Sec. 5).
- We propose a consistent coupling of bulk and (free) surface based on physical entities (Sec.4).
- Based on the coupling, a conservative formulation of surface dynamics is presented (Sec. 6).
- We apply our SPH-based model to simulate dynamics of diffusion effects and of a specific example of reaction kinetics, i.e. detergents in combination with a cleansing action on fluid-rigid interfaces (Sec. 7).

In Sec. 8 we show the versatility and the performance of our fully GPU-based implementation in various simulation scenarios. Sec. 9 draws some final conclusions.

2 Related Work

Since its introduction [Gingold and Monaghan 1977; Lucy 1977], SPH has been heavily used for simulation of fluids and we refer the reader to the surveys of Monaghan [2005] and Koumoutsakos et al. [2008] for a general overview.

2.1 Convection-Diffusion

In Computer Graphics, compact smoothing kernels [Müller et al. 2003], adaptive sampling [Adams et al. 2007; Solenthaler and Gross 2011; Orthmann and Kolb 2012] and parallelization [Kolb and Cuntz 2005; Goswami et al. 2010; Ihmsen et al. 2011b] are essential in order to reduce overall simulation times. Incompressibility is enforced by using a predictive-corrective formulation [Solenthaler and Pajarola 2009] in combination with adaptive time steps [Ihmsen et al. 2010]. In order to prevent undesirable pressure variations in combination with large density contrasts [Solenthaler and Pajarola 2008] or with rigid bodies [Akinci et al. 2012b] it is preferable to replace the density summation [Müller et al. 2003] by computation of a particle’s number density [Hu and Adams 2006]. Beside convection, a diffusive flux simulates thermodynamics [Müller et al. 2005] and defines transport of sediments [Kristof et al. 2009] or soluble substances [Cleary and Monaghan 1999; Monaghan 2005].

2.2 Surface Definitions

Interfaces can be identified using color gradient methods [Müller et al. 2003; Keiser et al. 2006; Akinci et al. 2012a]. In order to stabilize the formulation of surface tension, Solenthaler et al. [2008] employed an additional normalization. However, a second phase is required for gradient-based methods. As stated by Becker and Teschner [2007], derivatives of the color-gradient are sensitive to irregular particle structures. Thus, using ghost particles [Schechter and Bridson 2012] in order to emulate a second phase would result in unstable surface definitions. Our approach describes a stable surface definition which works on both, interfaces and free surfaces. For a more stable representation of free surfaces, signed distance functions are used [Solenthaler et al. 2007b; Adams et al. 2007]. These functions are employed to render smooth surfaces [Zhu and Bridson 2005; Solenthaler et al. 2007a; Onderik et al. 2011] and enable the computation of anisotropy information [Yu and Turk 2010]. However, these methods aim for surface reconstruction or capturing [Hieber and Koumoutsakos 2005]. In contrast, we define an implicit surface which is capable of simulating surface dynamics.

Losasso et al. [2008] propose particle level-set methods in order to track the surface of a fluid. However, our approach has the advantage that the surface definition is directly deduced from SPH particles, avoiding additional surface representations and particle re-seeding.

2.3 Multi-Phase Effects

SPH has been used in a variety of multi-phase effects, ranging from temperature modulated viscosity for lava flows [Stora et al. 1999], melting and solidification of objects [Solenthaler et al. 2007a] and melting and freezing of ice objects including a heat transfer steering the phase transition [Iwasaki et al. 2010]. Beside phase transitions, simulations of trapped air [Müller et al. 2005], bubbles [Hong et al. 2008; Ihmsen et al. 2011a] and diffuse materials [Losasso et al. 2008; Ihmsen et al. 2012] have enriched SPH effect simulations which circumvent problems induced by large density contrasts [Solenthaler and Pajarola 2008]. Other research deals with wetting effects for granular materials [Rungjiratananon et al. 2008; Lenaerts and Dutré 2009] and physically-based erosion of terrains [Kristof et al. 2009]. A fluid-rigid coupling has been achieved by using distance fields [Harada et al. 2007], via direct forcing [Becker et al. 2009], or more consistently by considering relative contributions of inhomogeneously sampled rigid particles [Akinci et al. 2012b]. However, none of the proposed methods simulates a quantity transport on phase interfaces. In computational physics, Adami et al. [2010] presented an SPH-based approach for surfactant dynamics, which however, is not applicable to free-surface scenarios and requires complex corrections of interface dynamics. In contrast, we utilize an implicit signed distance function [Zhu and Bridson 2005] in order to explicitly integrate a surface delta-function, which leads to consistent bulk and surface representations and supports simple dynamics on free surfaces as well as phase interfaces.

3 SPH Background

In this section we give a short introduction to the fundamental building blocks as necessary for a quantity transport on fluid surfaces.

3.1 Field Reconstruction

In SPH, as introduced by Gingold and Monaghan [1977] and Lucy [1977], a quantity field S is reconstructed over all particles j in the local neighborhood of sampling position \mathbf{x} :

$$S(\mathbf{x}) = \sum_j S_j V_i W_j(\mathbf{x}) \quad (1)$$

where $W_j(\mathbf{x}) = W(r, h) = W(\|\mathbf{x} - \mathbf{x}_j\|, h)$ (or in short W_{ij} for $S_i = S(\mathbf{x}_i)$) is a radial symmetric smoothing kernel [Müller et al. 2003] with compact support h and V_i is a particle’s dynamic volume. Assuming constant rest density ρ_0 [Akinci et al. 2012b; Solenthaler and Pajarola 2008] leads to the concept of particle number density $n_i = \sum_j v_j W_{ij}$. As a result, $V_i = \frac{m_i}{\rho_i} = \frac{\rho_0 v_i}{\rho_0 n_i} = \frac{v_i}{\rho_i}$, where v_i is a particle’s constant rest volume. Usually, a particle’s number density is $n_i \approx 1$ for incompressible particle configurations. Thus, to correct the neighbor deficiency close to free surfaces we enforce $n_i \geq 1$. However, in order to establish quantity fields on a surface, we still need to model the singularity at the surface.

3.2 Implicit Surface Definition

In general, the free fluid-air interface $\partial\Omega := \{\mathbf{x} \mid \phi(\mathbf{x}) = 0\}$ is defined as the zero iso-contour of the following signed distance func-

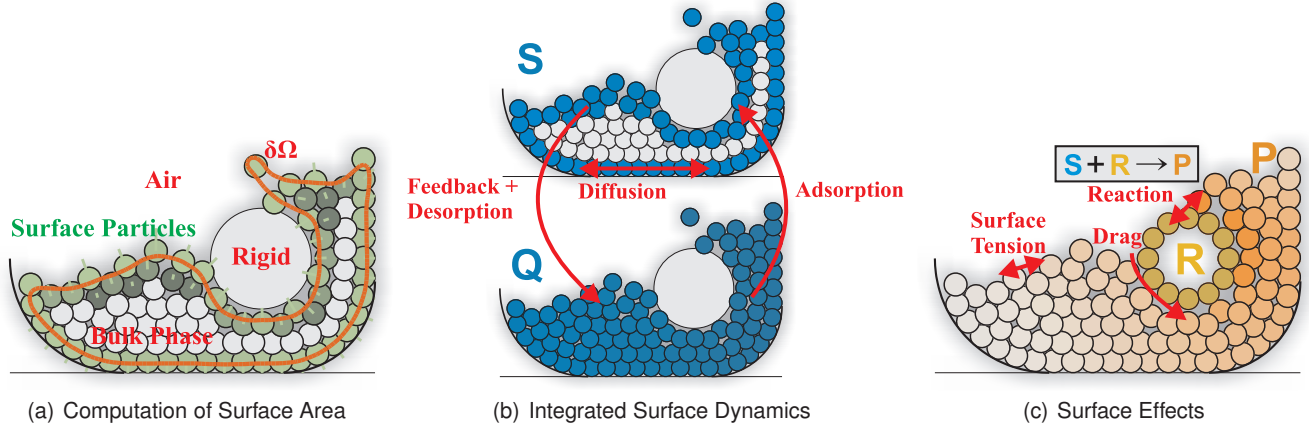


Figure 2: Simulation overview: fluid particles compute the surface area a_i (green) as defined by $\delta\Omega$ (see Fig. 2(a)). Surface particles, i.e. particles for which $a_i > a_{\min}$, constitute a surfactant field S on the surface (see Fig.2(b)), which changes due to diffusion along the surface and which interacts with a surfactant field Q in a fluid's bulk due to adsorption and desorption. Surface particles also feedback surfactant concentration when they return to the bulk. As shown in Fig. 2(c), in our simulation, surfactants S react with substances R (yellow) carried by rigid particles resulting in products P (orange) which dissolve into the bulk. Additionally, surfactant concentration influences surface tension and fluid drag.

181 tion [Zhu and Bridson 2005]:

$$\phi(\mathbf{x}) = \|\mathbf{x} - \mathbf{m}(\mathbf{x})\| - d, \quad (2)$$

where d is the desired distance between interface and particles, which in our simulation equals the particle's radius, and $\mathbf{m}(\mathbf{x})$ is the center of the local iso-density distribution [Onderik et al. 2011]:

$$\mathbf{m}(\mathbf{x}) = \frac{\sum_j \mathbf{x}_j V_j W_j(\mathbf{x})}{\sum_j V_j W_j(\mathbf{x})}.$$

182 Still, we need to find a representation which is capable of simulating
183 dynamics on the surface and of robust surface computation.

184 4 Coupling of Bulk and Surface

185 Some substances, like surface active agents, i.e. surfactants, which
186 are immersed in a fluid's bulk adhere to a fluid's surface. Conse-
187 quently, to simulate surface dynamics, as summarized in Fig. 2, we
188 need a robust and reliable estimation of the surface area. Accord-
189 ing to Bertalmio et al. [2001], it is advantageous to embed a lower
190 dimensional surface in a higher dimensional volume. Hence, our
191 idea is to sample the iso-contour as defined in the last section with
192 SPH particles resulting in surface areas a_i . Similar to Adami et
193 al. [2010], the underlying Lagrangian SPH simulation then acts as a
194 "particle-pool" but for quantity fields defined on surfaces, as shown
195 in Fig. 2(a).

196 Particles are divided into two groups. Particles within a small layer
197 around the surface, which we call *surface particles* (green) and all
198 other particles, called *bulk particles* (white). Surface particles have
199 a double role during simulation (Fig. 2(b)): they constitute a quan-
200 tity field S on the surface and at the same time, like bulk particles,
201 they contribute to a quantity field Q . Even if our method is not re-
202 stricted to scalar quantities, we consider $Q_i = \frac{\bar{Q}_i}{v_i}$ given in $[\frac{mol}{m^3}]$
203 and $S_i = \frac{\bar{S}_i}{a_i}$ given in $[\frac{mol}{m^2}]$ as concentrations of a soluble sub-
204 stance, e.g. concentration of detergent with a constant total molar
205 mass of $\sum_i \bar{Q}_i + \bar{S}_i$. Please note the difference between mass \bar{S}_i
206 and concentration S_i .

207 While \bar{Q} is trivially conserved in Lagrangian systems, including
208 matter diffusion [Monaghan 2005] and passive transport with fluid
209 particles [Solenthaler and Pajarola 2009; Akinci et al. 2012b], a
210 quantity flux from Q to S and inside S requires special symmetriza-
211 tion mechanisms (see Sec. 6). Beside surface dynamics, our method
212 is applicable for dynamics on phase interfaces as well, e.g. enabling
213 a cleansing action of S with a substance R given in $[\frac{mol}{m^2}]$ on rigid
214 surfaces (see Fig.2(c)). Additionally, a surfactant concentration on
215 the surface may alter fluid drag as induced by rigid objects or sur-
216 face tension, thus directly affects the underlying flow field.

217 Unlike particle volumes v_i , a particle's fraction of surface area a_i
218 is not constant due to internal and external forces changing the sur-
219 face topology i.e. particles may move closer to or further away from
220 the surface. Consequently, in order to reconstruct concentration
221 fields S , we need to compute the surface area at particle locations
222 as described in the following section.

5 Computation of Surface Area

224 The strength of our implicit surface definition is that quantity fields
225 S on a surface can be reconstructed over the fluid volume using
226 Eq. (1) leading to a consistent representation of bulk and surface.
227 However, relative concentrations S_i are defined with respect to a
228 particle's fraction of the surface area. In SPH, a surface integral
229 over the fluid volume Ω reads

$$a(\mathbf{x}) = \int_{\Omega} \delta(\phi(\mathbf{x}')) W(\|\mathbf{x} - \mathbf{x}'\|, h) d\mathbf{x}', \quad (3)$$

230 where $\delta(\phi(\mathbf{x}'))$ is the surface delta function and where we ap-
231 ply the assumption that $\|\nabla\phi(\mathbf{x})\| = 1$ common to level-set ap-
232 proaches [Osher and Fedkiw 2002], which for a regularly sampled
233 and incompressible SPH is a true assumption as well. As shown in
234 Fig. 3, a discretization of the delta function as described in Sec. 5.1
235 results in a narrow band of contributing particles. Each such parti-
236 cle represents a fraction of surface area, depending on its distance
237 to the surface as described in Sec. 5.2. In order to enable stable
238 dynamics (see Sec. 6) we correct delta values in singular regions
239 as described in Sec. 5.3 and make use of temporal coherence as
240 described in Sec. 5.4.

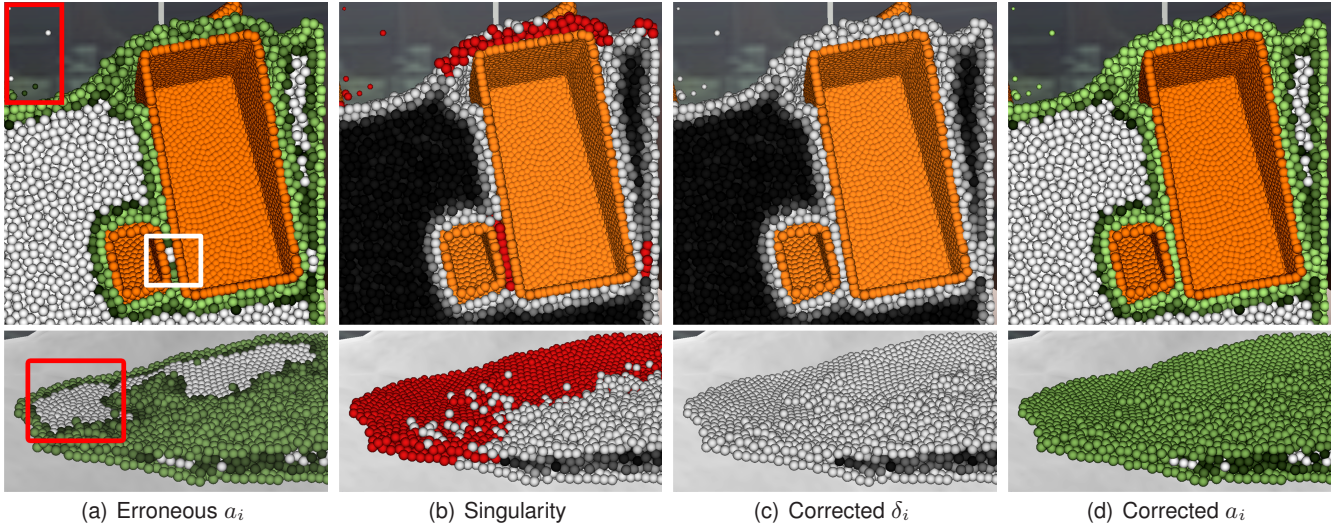


Figure 3: Computation of surface area for two particle configurations showing surface particles (green), bulk particles (white) and rigid particles (orange). No check for singularity and no normalization lead to erroneous area values a_i (highlighted regions in 3(a)). Instead, a detection of singular regions (red in 3(b)) enables a correction of delta values δ_i (increasing from black to grey in 3(b) and 3(c)), which are integrated to area values a_i (3(d)) using a corrected SPH interpolation (Eq. (5)).

5.1 Approximation of the Surface Delta Function

In order to determine the contribution of particles to the (free) surface, we smear out the iso-contour $\delta\Omega$ over the local fluid volume using SPH smoothing kernels. However, using a standard SPH kernel to approximate a surface delta function imposes several issues:

1. In combination with small support radii, Eq. (2), may return slightly fluctuating distance values ϕ_i . The resulting time-variance would then additionally be emphasized by higher order kernels.
2. Unlike level set methods, the surface $\partial\Omega$ is only sampled in the fluid Ω^- as shown in Fig. 4.

Regarding stable distance and quantity fields, we aim at low-order kernels, additionally reducing computation times. The lack of particles in Ω^+ requires an adjustment of the smoothing kernel in order to satisfy delta-function properties. Assuming that the surface is locally planar, which is a true approximation in the limit $\lim_{h \rightarrow 0}$, the contribution of fluid particles simply doubles, in order to compensate contributions from non-existing particles in Ω^+ . Thus, we approximate the surface delta function by a half-sided tent-kernel:

$$\delta(\phi) = \begin{cases} 2(1 + \frac{\phi}{d}) & \text{if } \phi < 0 \\ 0 & \text{otherwise,} \end{cases} \quad (4)$$

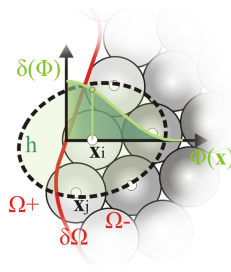


Figure 4: Sampling of the surface using a half-sided smeared out delta function approximation.

which depends only on the distance to the iso-contour at $\phi(\mathbf{x}) = 0$ for which by definition $\phi(\mathbf{x}) \geq -d$ holds. During simulation we integrate discrete values $\delta_i = \delta(\phi(\mathbf{x}_i))$ evaluated at particle locations in order to compute a surface area.

5.2 Interpolation of Particle Areas

Particles close to the surface have a high contribution. The closer a particle, the more it contributes to the surface (color coded from dark to light green in Fig. 3(d)). In order to determine how much of the surface area is represented by a particle, we have to integrate the surface delta function as derived in the last section over a particle's support h (see Fig. 4). In detail, the corresponding SPH summation for Eq. (3) yields

$$a_i = \sum_j \delta_j V_j \overline{W}_{ij}, \quad (5)$$

where $\delta_i = \delta(\phi(\mathbf{x}_i))$ is the delta function evaluated at position $\mathbf{x}_i \in \Omega^-$. Due to the empty neighborhood in Ω^+ we have to correct the resulting volume deficiency by using an adapted weighting kernel [Bonet and Kulasegaram 2002]:

$$\overline{W}_{ij} = \frac{W_{ij}}{\sum_j V_j W_{ij}}.$$

Such a normalization also ensures that area values smoothly change between neighboring particles. Due to the definition of the distance function (Eq.(2)), a disturbance of regular particle structures, as caused by the flow-field, leads to small area values in the fluid bulk. Thus, we consider the particle to be a bulk particle (white particles in Fig. 3(d)) as long as a particle's area is below or equal a_{\min} . However, values δ_i may also be incorrect in under-resolved regions as described in the next section.

5.3 Thin Fluid Sheets

Quantity fields on the surface require stable area values. However, within thin fluid sheets regular but deficient particle neighborhoods can emerge which might lead to erroneous area values as shown in

284 Fig. 3(a). Singular cases can be identified by setting a lower thresh- 326
 285 old for the number of neighboring particles, but dense and strongly 327
 286 anisotropic distributions remain unidentified. A better description 328
 287 for local particle distributions is the weighted covariance matrix of 329
 288 a particle i , given as [Yu and Turk 2010]

$$\mathbf{C}_i = \frac{\sum_j (\mathbf{x}_j - \mathbf{m}_i)(\mathbf{x}_j - \mathbf{m}_i)^T W_{ij}}{\sum_j W_{ij}} \in \mathbb{R}^{3 \times 3}. \quad (6)$$

289 Since we want to detect singular particle structures, the determi- 330
 290 nant of a particle's covariance matrix naturally reveals flat or planar 331
 291 particle neighborhoods. Accordingly, if $|\mathbf{C}_i| < \epsilon_c$ or if a particle 332
 292 i has less than 30 neighbors (red particles in Fig. 3(b)) we will set 333
 293 $\delta_i = \delta_{\max}$ leading to a corrected approximation of delta values as 334
 294 shown in Fig. 3(c).

295 5.4 Temporal Coherence

296 In order to stabilize quantity fields, particle areas should change 335
 297 smoothly over time. Fortunately, due to the temporal coherent na- 336
 298 ture of particle systems, we can apply a temporal smoothing of par- 337
 299 ticle areas, which is computed as

$$\delta_i(t+1) = (1 - \kappa)\delta_i(t) + \kappa\delta_i(t+1)^*, \quad (7)$$

300 where $\delta_i(t+1)^*$ is the approximated surface delta function ac- 344
 301 cording to Eq. 4 and where κ defines the rate of adjustment to new 345
 302 values $\delta_i(t+1)^*$. In all our examples $\kappa = 0.1$ resulted in smooth 346
 303 transitions.

304 In regions with little velocity divergence, i.e. where $\nabla \cdot \mathbf{u}_i < \epsilon_u$, we 347
 305 recompute $\delta_i(t+1)^*$ only every 10-th frame. This is valid, since 348
 306 in these regions $\frac{\partial}{\partial t}\delta_i = 0$ holds (see App. A).

307 6 Conservative Surface Dynamics

While mass transport in a fluid's bulk has been subject of many 349
 applications, a coupling of the bulk with a surface and dynamics 350
 on fluid surfaces have not been investigated yet. Depending on the 351
 simulated physics, interfacial quantity fields change due to a mass 352
 flux between neighboring particles:

$$\frac{\partial}{\partial t} S_i = \frac{1}{a_i} \sum_j \Gamma_{i \leftarrow j},$$

308 where $\Gamma_{i \leftarrow j}$ represents a mass flux from particle j to particle i . 360
 309 Most importantly, such pairwise contributions must be symmetric 361
 310 in order to satisfy mass conservation, i.e. $\Gamma_{i \leftarrow j} = -\Gamma_{j \leftarrow i}$. In this 362
 311 section we therefore develop the building blocks for a conservative 363
 312 transport between bulk and surface and for dynamics on surfaces as 364
 313 well as phase interfaces for which we give examples in the context 365
 314 of surfactant dynamics.

315 6.1 Consistent Transport between Bulk and Surface

316 Dynamics of a fluid's bulk and surface are strongly interconnected. 366
 317 For example, surfactants like detergents, which adhere to a fluid's 367
 318 surface, usually originate from a fluid's bulk and may return to it. 368
 319 Thus, mass is transferred between two different kinds of particle 369
 320 fields, surface particles i and bulk particles j (which might be one 370
 321 and the same particle, i.e. $i = j$, but in different roles). Conse- 371
 322 quently, a transport mechanism between bulk and surface is not 372
 323 symmetric per se. To ensure conservation, we compute a quantity 373
 324 flux with focus on surface particles i and assume the opposite flux 374
 325 for bulk particles j :

$$\frac{\partial}{\partial t} S_i = \frac{1}{a_i} \sum_j \Gamma_{i \leftarrow j}, \quad \text{and} \quad \frac{\partial}{\partial t} Q_j = \frac{1}{v_j} \sum_i -\Gamma_{i \leftarrow j}. \quad (8)$$

where $\Gamma_{i \leftarrow j}$ are defined with respect to absolute quantities, 326
 i.e. $\bar{S}_i = a_i S_i$ and $\bar{Q}_i = v_i Q_i$. That way we take as much of a 327
 substance from the fluid bulk as the surface receives and vice versa. 328

329 6.1.1 Adsorption and Desorption

330 The driving mechanism for our simulation of surface dynamics 331
 is the well known Langmuir-Hinshelwood mechanism [Rosen and 332
 Kunjappu 2004] which describes how much of a so-called "free" 333
 substrate or target Q_j in a carrier fluid is adsorbed on a surface as 334
 shown in Fig. 5. The net rate of adsorbed substrates at surface parti- 335
 cle i mainly depends on the presence of targets at neighboring bulk 336
 particles j :

$$\Gamma_{i \leftarrow j}^a = [\sigma_a \bar{Q}_j (\bar{S}_0 - \bar{S}_i) - \sigma_f \bar{S}_i] V_j W_{ij}, \quad (9)$$

337 where σ_a defines the speed of adsorption and where the total num- 338
 ber of available capture sites \bar{S}_0 limits the adsorption process. Over 339
 time adsorbed targets constantly dissociate from the surface as con- 340
 trolled by σ_f . The desorption rate usually is much smaller than the 341
 adsorption rate, i.e. $\sigma_a \gg \sigma_f$. The larger σ_f , the less saturated the 342
 surface becomes. Fig. 5 shows the importance of adsorption for a 343
 falling drop of detergent.

344 6.1.2 Feedback

345 Beside physically-based mass transport between bulk and surface, 346
 we account for particles which move away from the surface, i.e. for 347
 which a_i drops below a_{\min} . Such (former) surface particles have to 348
 transfer mass back to the bulk in order to conserve the total number 349
 of surfactant molecules in the system. Naturally, such a feedback 350
 from surface particles i to bulk particles j is a much faster desorp- 351
 tion process. Thus, we return mass by increasing σ_f and setting 352
 $\sigma_a = 0$ for particles returning to the bulk. In order to avoid nu- 353
 merical problems due to decreasing area values during feedback, 354
 we keep $a_i = a_{\min}$ until all surface quantity is transferred back to 355
 nearby bulk particles. Particles returning to the bulk are excluded 356
 from surface dynamics.

357 6.2 Unified Free-Surface and Interface Dynamics

358 In SPH, contributions between bulk particles usually are sym- 359
 metrized using gradient approximations [Colin et al. 2006] or in- 360
 tegral approximations [Cleary and Monaghan 1999] making use of 361
 constant rest volumes. Due to non-constant particle areas, standard 362
 symmetrization techniques do not lead to symmetric formulations 363
 for surface dynamics. Therefore, we enforce conservation explic- 364
 itly by averaging pairwise contributions between interface particles, 365
 i.e. using the identity $\Gamma_{i \leftarrow j} = -\Gamma_{j \leftarrow i}$:

$$\frac{\partial}{\partial t} S_i = \frac{1}{a_i} \sum_j \Gamma_{i \leftarrow j} = \frac{1}{a_i} \sum_j \frac{1}{2} [\Gamma_{i \leftarrow j} - \Gamma_{j \leftarrow i}], \quad (10)$$

where i and j might also be part of different phases. As spe- 366
 cific kinds of surface dynamics we introduce diffusion on a surface 367
 (Sec. 6.2.1) and a reaction kinetics (Sec. 6.2.2). 368

369 6.2.1 Diffusion

370 Once surfactants have been adsorbed at the surface, they are trans- 371
 ported along the tangential direction of the surface. Since S is non- 372
 zero only at the surface, we can approximate a diffusion of surfac- 373
 tants as (see App.B)

$$\Gamma_{i \leftarrow j}^d = \sigma_d (S_i - S_j) (a_i V_i + a_j V_j) \frac{\partial}{\partial r} W_{ij}, \quad (11)$$

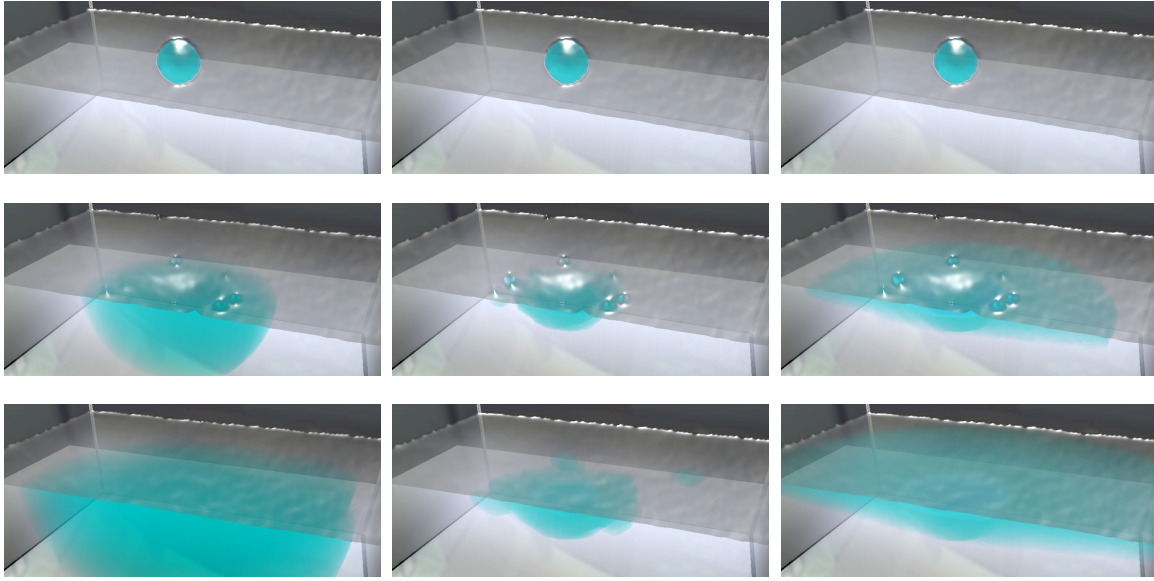


Figure 5: A falling drop of detergent shown for three different time steps (rows) and for different adsorption σ_a and diffusion constants σ_d (columns). No adsorption $\sigma_a = 0$ leads to diffusion in the bulk (left column), while $\sigma_a > 0 \wedge \sigma_d = 0$ leads to a local concentration on the surface (middle column). In contrast, $\sigma_a > 0 \wedge \sigma_d > 0$ results in homogeneous concentration of surfactant on the surface (right column).

where σ_d is an isotropic diffusion constant. Please note that i, j need to be restricted to surface particles in order to avoid diffusion into the fluid bulk, leading to a homogeneous surfactant concentration on the surface (see Fig. 5).

6.2.2 Reaction Kinetics

In reaction kinetics like the cleansing action of detergents, as shown in Fig. 1, surfactants S react with a substance R on rigid surfaces given in $[\frac{mol}{m^2}]$ forming products or micelles P which directly dissolve into the bulk given in $[\frac{mol}{m^3}]$. We describe reaction kinetics such a cleansing processes, as a simple forward reaction [Berthier and Silberzan 2009], consisting of a single bimolecular reaction $\alpha_S \bar{S} + \alpha_R \bar{R} \rightarrow \alpha_P \bar{P}$, where α_S, α_R and α_P are stoichiometric coefficients, which define how much reactant molecules \bar{S} and \bar{R} are irreversibly consumed in order to form product molecules \bar{P} , e.g. micelles in case of cleansing. Here, $\bar{S}, \bar{R}, \bar{P}$ stand for a constant molar mass of the respective substance. By enforcing symmetry as defined via Eq. (8), the reaction rate for fluid particles i and rigid particles k is

$$\frac{1}{\alpha_P} \frac{\partial \bar{P}_i}{\partial t} = -\frac{1}{\alpha_S} \frac{\partial \bar{S}_i}{\partial t} = -\frac{1}{\alpha_R} \frac{\partial \bar{R}_k}{\partial t} = \sum_k \Gamma_{i \leftarrow k}^r.$$

In our examples we set $\alpha_S = \alpha_R = \alpha_P = 1$. Please note that, since the product mass, e.g. micelles, directly dissolve into the fluid bulk, $\bar{P}_i = v_i P_i$ holds, whereas $\bar{S}_i = a_i S_i$ and $\bar{R}_k = a_k R_k$ are defined with respect to areas of fluid particles a_i and areas of rigid particles a_k . Since rigid particles directly sample a rigid's surface, we pre-compute a_k with Eq.(5) using $\delta_k = \delta_{max}$.

The speed of the reaction is defined via a simple rate law and is proportional to $\sigma_r \bar{S}_i \bar{R}_k$, i.e. it linearly depends on the rate constant σ_r and the total number of molecules of both reactants. Thus, the reaction is formulated as

$$\Gamma_{i \leftarrow k}^r = \sigma_r \bar{S}_i \bar{R}_k \frac{1}{2} (V_i + V_k) W_{ij}, \quad (12)$$

by using Eq. (10).

Please note that for adjacent phases iso-contours do in general not match exactly (see Eq.(2)). However, pairwise averaging of contributions as done in Eq. (12) naturally corrects such a discontinuity and leads to a unified simulation capable of computing dynamics for free surfaces as well as phase interfaces.

7 Implementation Details

For clarity we outline our fully GPU-based implementation of surface dynamics in Alg. 1 and refer to SPH literature for mass transport of Q in the bulk, including neighbor finding [Green 2009], an incompressible convection [Solenthaler and Pajarola 2009] coupled with rigid objects [Akinci et al. 2012b] and matter diffusion [Monaghan 2005]. Surfactant concentration linearly alters the surface tension coefficient as proposed by Becker and

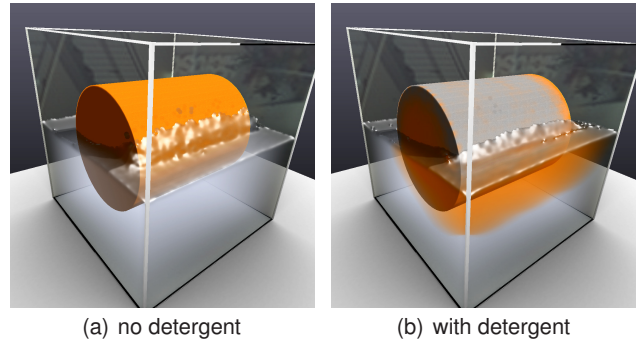


Figure 6: Rotating cylinder before (6(a)) and after (6(b)) drops of detergent have been added. No detergent concentration leads to strong drag and surface tension effects corresponding to a real surface effect, as described by Fell [2011], while detergents clean the cylinder's surface and reduce fluid drag.

Algorithm 1: Data-Parallel Surface Dynamics	
Delta Function	
foreach fluid particle i where $\nabla \cdot \mathbf{v}_i(t) > \epsilon_u$ inparallel do	<ul style="list-style-type: none"> └ compute $\phi_i(t)$ using a support of $2.5h$ (Eq. (2)) └ estimate $\delta_i(t)^*$ (Eq. (4))
foreach fluid particle i where $\nabla \cdot \mathbf{v}_i(t) > \epsilon_u$ inparallel do	<ul style="list-style-type: none"> └ compute $\mathbf{C}_i(t)$ using a support of $2.5h$ (Eq. (6)) └ if $(\mathbf{C}_i(t) < \epsilon_c \parallel \text{NumNeighs} < 30) \delta_i(t)^* = \delta_{\max}$
foreach fluid particle i inparallel do	<ul style="list-style-type: none"> └ update $\delta_i(t)$ (Eq. (7))
Surface Area	
foreach fluid particle i inparallel do	<ul style="list-style-type: none"> └ compute $a_i(t)$ (Eq. (5)) └ if $(a_i(t) > a_{\min})$ mark i as surface particle
Adsorption and Feedback (Eq. (9))	
foreach surface particle i inparallel do	<ul style="list-style-type: none"> └ $\frac{\partial}{\partial t} S_i = \frac{1}{a_i} \sum_j \Gamma_{i \leftarrow j}^a$
foreach fluid particle i inparallel do	<ul style="list-style-type: none"> └ $\frac{\partial}{\partial t} Q_i = \frac{1}{v_i} \sum_j -\Gamma_{j \leftarrow i}^d$
Diffusion (Eq. (11))	
foreach surface particle i inparallel do	<ul style="list-style-type: none"> └ $\frac{\partial}{\partial t} S_i += \frac{1}{a_i} \sum_j \Gamma_{i \leftarrow j}^d$
Reaction (Eq. (12))	
foreach surface particle i inparallel do	<ul style="list-style-type: none"> └ $\frac{\partial}{\partial t} S_i += \alpha_S \frac{1}{a_i} \sum_k \Gamma_{i \leftarrow k}^r$
foreach rigid particle k inparallel do	<ul style="list-style-type: none"> └ $\frac{\partial}{\partial t} R_k = \alpha_R \frac{1}{a_k} \sum_k \Gamma_{i \leftarrow k}^r$
foreach fluid particle i inparallel do	<ul style="list-style-type: none"> └ $\frac{\partial}{\partial t} P_i = \alpha_P \frac{1}{v_i} \sum_k -\Gamma_{i \leftarrow k}^r$

Scene	"Pan"	"Flooding"	"Cylinder"	"Kinect®"
σ_r/σ_d	10/10	70/10	40/10	40/10
σ_a/σ_f	10/0.1	10/0.1	10/1.0	10/0.1
Snapshot t_{sim}	23 sec.	30 sec	3 sec	20 sec
Avg. δt [ms]	2	1.5	2	1.5
# fluid ptcls	541k	1.1M	891k	750k
# surface ptcls	142k	200k	152k	300k
Delta Func. [ms]	14.2	30.2	21.7	60.0
Surface Area [ms]	7.4	14.8	12.8	9.2
Adsorption [ms]	10.1	19.0	16.1	14.9
Diffusion [ms]	1.9	2.8	2.2	3.6
Reaction [ms]	9.0	17.5	15.2	12.0
Time per Frame	160	261	227	252

Table 1: GPU timings (in msec) for operations as given in Alg.1.

around 30 neighbors per particle in combination with smoothing kernels as proposed by Müller et al. [2003]. However, for the computation of the distance information and the covariance matrix we increase the smoothing radius to $2.5h$ to obtain reliable results. Except the velocity divergence threshold ϵ_u , all constants necessary to compute surface areas, i.e. the minimal surface area a_{\min} , the max delta function value δ_{\max} , and the threshold for the determinant of the covariance matrix ϵ_c , are pre-computed from pre-defined incompressible particle configurations as shown in Fig. 7. Thus, a users get an intuitive way to define constants. For more details, see the accompanying 2D Matlab® implementation which has been used to generate Fig. 2.

8 Results and Discussion

We have tested our method in various scenarios in order to show its versatility, including the washing of dishes (Fig. 1), the wetting of a rotating cylinder (Fig. 6), the flooding of a valley (Fig. 10,3), a complex Kinect® scene (Fig. 8) and an evolution of a single drop of detergent (Fig. 5). For visualization of surfactant concentration we utilized an SPH-based volume rendering approach [Fraedrich et al. 2010] in combination with an image-based smoothing of particle surfaces [van der Laan et al. 2009]. The scenarios were simulated on an Intel Dual-Core 3.3 GHz with an NVidia GTX 580 with 1.5 GB VRAM, for which sample simulation timings are given in Tab. 1.

Due to increased smoothing radius during distance computation, our surface layer is two particles thick and computation of distance values becomes more time consuming. However, as described in Sec. 5.4, in regions with small velocity divergence we recompute the distance values only every 10 frames, which reduces the computational overhead.

Fig. 9 compares our surface area to the color gradient based interfaces used by Adami et al. [2010] (note, that we apply $2.5h$ sampling radius in contrast to $6h$ by Adami et al. [2010], which would lead to even thicker surface layers). Most importantly, our approach supports free surfaces. But even at phase interfaces our approach results in a much thinner band of contributing particles. Thus, our method avoids error-prone normal projection for surface dynamics as used by Bertalmio et al. [2001]; we do not require any normal computation. Additionally, color gradients are prone to irregular particle structures which requires a correction of differentials as also discussed by Becker and Teschner [2007].

In the teaser example in Fig. 1, dishes with a grease cover get exposed to incoming fluid with a constant detergent concentration of $Q = 1.0$. The underlying reaction kinetics transforms the grease R and the detergent S concentrated at the surface (Fig. 1, right), into reaction product P , i.e. solved grease / micelles in this case. The solved micelles diffuse in the bulk (Fig. 1, center).

Teschner [2007] and the drag coefficient similar to Akinci et al. [2012b] resulting in wetting effects as shown in Fig.6. We integrate a surfactant flux using an explicit Euler integration with adaptive time-steps [Ihmsen et al. 2010] which is sufficient for surface dynamics, since in scales of meters, diffusion always takes place at much smaller scale than convection. In case surfactant concentration does not influence convection, one may as well pre-compute a particle movement and use it as a base simulation for surface dynamics.

Beside attributes required for convection, we store surfactant masses \bar{Q} and \bar{S} , delta values δ_i and areas a_i as additional attributes per fluid particle. To avoid numerical problems with 32-bit floating point numbers we normalize the actual molecular mass of a particle with respect to a maximum mass \bar{S}_{\max} . Consequently, for $\bar{S}_{\max} = e^8$ a concentration of $S = 1.0$ represents a molecular mass of $e^8 \frac{\text{mol}}{\text{m}^3}$.

In all our examples, we set $h = 2d$, where d is a particle's radius, which results in a rest distance of $0.92h$ between particles and

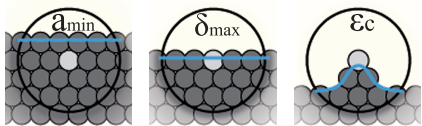


Figure 7: Constants are computed for reference particles (white) in user-defined particle configurations.



Figure 8: Complex room-scene which has been acquired with a Kinect[®] camera. Multiple material colors are washed out over time resulting in dirty water.

468 In the rotating cylinder example in Fig 6, three drops of detergent
 469 with $Q = 1.0$ are added after three seconds of simulation. Again,
 470 reaction kinetics take place at the cylinder surface, i.e. the added
 471 detergent leads to an wash-out effect. Additionally, detergent con-
 472 centration at the fluid-cylinder interface steers the dragging force
 473 implied to the fluid. Here, the high detergent concentration lowers
 474 the fluid’s drag.

475 In Fig. 8, we apply our SPH-based surface dynamics to a complex
 476 scene with highly irregular point distribution originating from
 477 a Kinect[®] sensor. We use the acquired point colors as substance R to
 478 be washed out from the fluid poured into the scene with a detergent
 479 concentration of $Q = 1.0$.

480 The flooding valley example in Fig. 10 illustrates the influence of
 481 surface dynamics on dynamic rigid objects in the fluid. Again, two
 482 different detergent concentrations are used in the incoming fluid,
 483 $Q = 0.05$ (Fig. 10, top row) and $Q = 1.0$ (Fig. 10, bottom row).
 484 As in the cylinder example in Fig. 6, detergent concentration at the
 485 fluid-rigid interface take part in the reaction kinetics, i.e. the wash-
 486 out effect, and on the dragging at this interface. Whereas in an
 487 early state, the scene layout is very similar (Fig. 10, left column),
 488 the dynamic dragging and surface tension leads to a very different
 489 outcomes later on (Fig. 10, right column).

490 Currently, the main limitation of our implementation is that the sur-
 491 face resolution is directly linked with the bulk resolution, since we
 492 use a homogeneous particle size. However, in specific situations,
 493 the accuracy for surface area measures and surface thickness should

be higher than the bulk resolution, as can be seen in the rotating
 cylinder example in Fig. 6. This limitation can be solved by adap-
 tive particle resolutions at fluid surfaces as introduced by Orthmann
 and Kolb [2012] or by utilizing a multi-scale approach [Solenthaler
 and Gross 2011]. Another limitation is the simplicity of the reac-
 tion kinetics, which does not account for temperature dependencies
 or more complex, non-linear reactions like explosions.

We also refer to the additional video for better impression on the
 dynamics of our method.

9 Conclusion

We presented a novel approach for robust computation of fluid
 (free) surfaces, which is the core concept for any physically based
 simulation of surface dynamics. We introduced a consistent and
 conservative formulation for interaction within a fluid surface and
 for adsorption-based interaction between fluid surface and bulk.
 Based on this formulation, we presented a diffusion model which
 incorporates different diffusion behavior for surface and bulk, as
 well as a model for reaction kinetics taking place at fluid-rigid sur-
 faces. A specific example for reaction kinetics, i.e. surface cleaning
 is introduced as well. We evaluated our approach using various ex-
 ample scenarios.

Our surface dynamics approach can easily be enriched with other
 effects like foam dynamics, temperature dependant or non-linear
 reactions.

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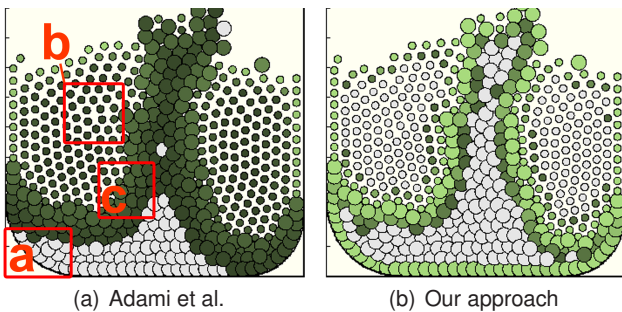


Figure 9: Comparison to color-gradient based interface approx-
 imation by Adami et al. [2010] (sampling radius $2.5h$): Our ap-
 proach handles free-surface (e.g. region a), irregular particle struc-
 tures (e.g. region b), and it results in thin interfaces (e.g. region c).

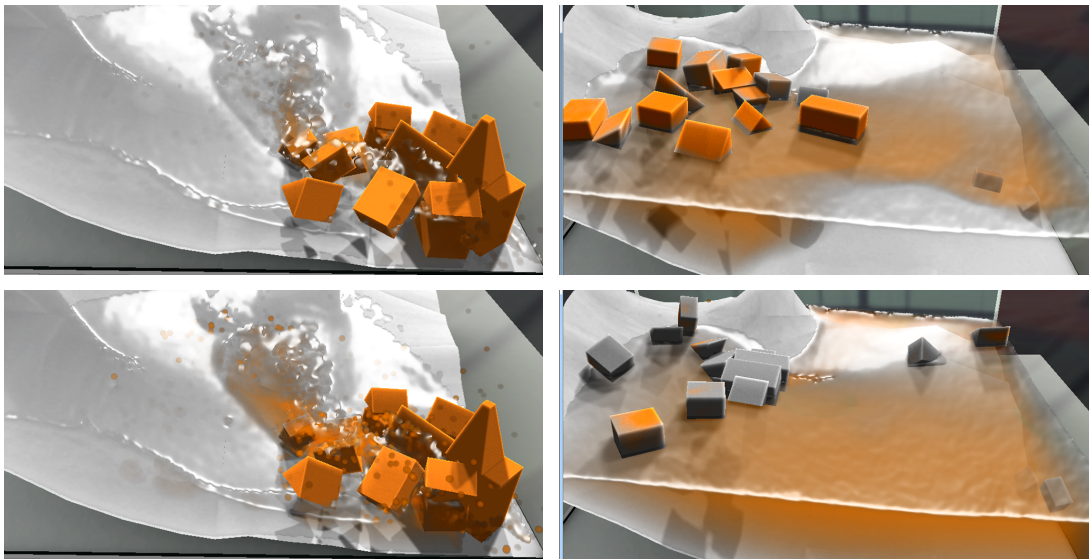


Figure 10: Flooding of a valley with dynamics rigid objects shown for two time-steps $t_{sim} = 6\text{ s}$ (left column) and $t_{sim} = 30\text{ s}$ (right column). In the upper row a fluid with detergent concentration $Q = 0.1$ is emitted while in the lower row the fluid is initialized with a concentration of $Q = 1.0$. Less detergent not only results in less cleansing but also results in a different convection of rigid objects.

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A Appendix: Temporal Coherence

A non-divergent and temporal coherent particle neighborhood, i.e. $\nabla \cdot \mathbf{u}_i = 0$ where velocities $\mathbf{u}_{ij} = \mathbf{u}_i - \mathbf{u}_j \approx \mathbf{0}$, leads to $\frac{\partial}{\partial t} W_{ij} = \mathbf{u}_{ij} \cdot \hat{\mathbf{r}}_{ij} \frac{\partial}{\partial r} W_{ij} \approx 0$. By applying this identity in combination with the quotient rule we get

$$\frac{\partial}{\partial t} \mathbf{m}_i = \frac{[\sum_j V_j \frac{\partial}{\partial t} (\mathbf{x}_j W_{ij})][\sum_j V_j W_{ij}] - [\sum_j V_j \frac{\partial}{\partial t} W_{ij}][\sum_j \mathbf{x}_j V_j W_{ij}]}{[\sum_j V_j W_{ij}]^2}$$

where $\frac{\partial}{\partial t} (\mathbf{x}_j W_{ij}) = \mathbf{u}_j W_{ij} + \mathbf{x}_j \frac{\partial}{\partial t} W_{ij} \approx \mathbf{u}_j W_{ij}$, which leads to

$$\frac{\partial}{\partial t} \mathbf{m}_i = \frac{[\sum_j \mathbf{u}_j V_j W_{ij}][\sum_j V_j W_{ij}]}{[\sum_j V_j W_{ij}]^2} \approx \mathbf{u}_i \frac{[\sum_j V_j W_{ij}][\sum_j V_j W_{ij}]}{[\sum_j V_j W_{ij}]^2} = \mathbf{u}_i.$$

668 for which directly follows that $\frac{\partial}{\partial t} \phi_i = \frac{\mathbf{x}_i - \mathbf{m}_i}{\|\mathbf{x}_i - \mathbf{m}_i\|} (\mathbf{u}_i - \frac{\partial}{\partial t} \mathbf{m}_i) = 0$.

669 Consequently, $\frac{\partial}{\partial t} \delta_i = \frac{\partial}{\partial \phi} \delta(\phi_i) \frac{\partial}{\partial t} \phi_i = 0$ as long as $\nabla \cdot \mathbf{u}_i = 0$.

B Appendix: Surface Diffusion

Starting with the integral approximation of second derivatives according to Cleary et al. [Cleary and Monaghan 1999]:

$$\nabla^2 S(\mathbf{x}_i) \approx 2 \int_{\Omega} (S(\mathbf{x}_j) - S(\mathbf{x}_i)) \frac{\partial}{\partial r} W_{ij} \partial \mathbf{x}_j,$$

we can approximate the Laplacian by integrating first order derivatives over the fluid volume Ω . Since S is non-zero only at the surface, we can approximate a diffusive mass flux on the surface as

$$\sigma_d \nabla^2 S_i \approx \frac{2}{a_i} \sum_j \Gamma_{i \leftarrow j} = \frac{2}{a_i} \sum_j \sigma_d (S_j - S_i) a_j V_j \frac{\partial}{\partial r} W_{ij},$$

where σ_d is an isotropic diffusion constant. However, since particle areas are not equal we do not get a conservative SPH approximation directly and need to enforce symmetry $\Gamma_{i \leftarrow j} = -\Gamma_{j \leftarrow i}$ explicitly by using Eq. (10):

$$\sigma_d \nabla^2 S_i \approx \frac{1}{a_i} \sum_j \sigma_d (S_i - S_j) [a_j V_j + a_i V_i] \frac{\partial}{\partial r} W_{ij},$$

671 which effectively averages a mass flux between surface particles.